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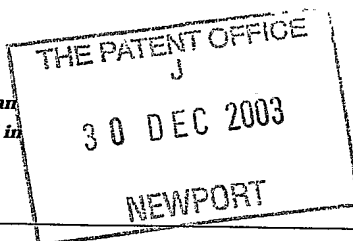
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MRH/P103062GB

30DEC03 EB62404-1 D02973

F01/7700 0.00-0330146.2 NONE

2. Patent application number

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30 DEC 2003

3. Full name, address and postcode of the or of each applicant (underline all surnames)

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Patents ADP number (if you know it)

7614282001

If the applicant is a corporate body, give the country/state of its incorporation

UK

4. Title of the invention

FORMATION OF GLASS FLAKES

5. Name of your agent (if you have one)

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Number of earlier application

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Description 6

Claim(s)

Abstract

Drawing(s) 3 *13*

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Priority documents

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Michael Harrison

29-12-03

12. Name and daytime telephone number of person to contact in the United Kingdom

Michael Harrison

0113 233 0100

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FORMATION OF GLASS FLAKES

Field of the Invention

The invention relates to methods for forming flakes or other small particles of glass or of other similar materials, including ceramic materials.

5 The present invention is applicable to any material which melts when heated and is capable of being formed into small entities such as flakes. Such material is being increasingly used for a variety of purposes including in paints, coatings, cosmetics, carpets, floor tiles and in thermoplastics. The flakes can be used to alter substantially the properties of the materials in which they are incorporated, for instance, by
10 altering their appearance, in particular the light reflective properties, and by improving the materials mechanical properties and also by increasing fire retardancy and smoke emissions.

Background to the Invention

15 In our European patent specification No 0 289 240 there is disclosed apparatus for forming flakes of material from a heated stream of molten material. The apparatus comprises means for feeding the stream in a downwards direction into a rotating cup, the cup being arranged with its open mouth facing upwardly such that molten material within the cup is caused to flow over the upper edges of the cup and flow
20 outwards in a radial direction due to centrifugal force. The apparatus also includes a pair of spaced apart substantially parallel plates arranged about the cup such that the material leaving the cup by centrifugal force passes through a gap defined between the plates. The plates are mounted within a vacuum chamber arranged such that a vacuum is applied to the space between the plates forming an annular venturi
25 drawing air from outside the chamber between the plates in a radial direction, maintaining angular velocity and preventing the molten material from touching the sides of the plates and cooling the material until reaches a solid state. The material is pulled at velocity by the air stream in an angular direction as the radius expands

thereby keeping it in the form of a flat film and ultimately breaking it into small platelets.

5 It is stated in EP 0 289 240 that by suitable choices of the speed of rotation of the cup, the distance between the two plates and the rate of air flow through the vacuum chamber, the size and thickness of the flakes of material to be produced can be changed and controlled. It is further stated that the apparatus may be used not only with glass but with materials such as basalt, ceramics such as alumina, graphite, and metals such as lead. For each different material it may be necessary to alter the operation of the apparatus by, for instance, varying the speed of rotation of cup, the temperature of the molten material, the size of the gap between the plates and the airflow between the plates. In a further reference to factors which may be varied, reference is made to the volume of molten stream entering the cup, the temperature of that material, the speed of the cup, the diameter of the cup, the distance between the cup and the plates and the airflow at the exit from the vacuum chambers associated with the plates.

20 As far as concerns the distance between the cup and the plates, there was no clear understanding of the effect of changing this distance. It was known that the distance could only be varied in both directions within certain parameters to produce flake rather than strands or fibres but the main effect was thought to be a reduced thickness of flake with increase in distance between the cup and the plates due to a longer period of stretching the glass before cooling and an increase in nominal flake diameter.

25 In practice, for some applications glass flakes are required with a particle thickness size distribution as narrow as possible, since this results in a product with the desired range of physical properties for further processing. In other applications a wide spread of particle size distribution may be required, for example to provide optical effects. However, there are, as indicated above, a substantial number of parameters affecting the nature of the product of which the cup plate separation represents only

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one possible variable. It was thought that the distance between cup and plates should be fixed at a median consistent with the production of acceptable flakes, with the parameters of thickness being changed by varying the plate gap, cup peripheral velocity and air flow. Any change of the cup to plate distance was thought simply to be an additional means of changing the thickness of the product but not of changing the thickness distribution.

Apparatus as described in EP 0 289 240 has been operated for many years on what was thought to be the most optimal combination of operating conditions in order to produce the best product. However, even under such conditions, glass flake is produced with a controlled thickness but quite a wide particle distribution range which was generally thought to be uncontrollable. For many applications, the size range required is outside that produced by such apparatus. Accordingly, the product has to be graded and the material at the bottom and top of the size range has to be removed and then discarded or recycled. This process increases the expense of producing the product and it would be desirable if a product could be produced with a more specific particle size range so that the extent of grading, discarding and recycling of products can be reduced or eliminated.

Statements of the Invention

According to the present invention there is provided a method of changing the particle thickness size distribution of flakes of material formed by a process which comprises feeding a stream of molten material in a downwards direction into a rotating cup or disc, and allowing the material to pass over the edge of the cup in such a manner as to be forced into the gap between a pair of plates surrounding the cup, the movement of the material being maintained in an angular direction and effected by a flow of air passing through the plates and either side of the material so as to pull the stream of material in such a manner as to keep it flat and also to pull it so that, as solidification of the material is effected, the sheet of material so formed is

broken into flakes, the method comprising varying the distance between the cup and entry to the plates until the desired particle size distribution is obtained.

5 Accordingly, the present invention provides a means whereby, in the production of glass flakes or other flake material, the relationship between the edge of the spinning cup or disc, instead of remaining fixed is changed, to produce a difference in particle thickness size distribution thus allowing production of discrete size distributions during the production phase rather than as a secondary production process.

10 Although it was previously known that variation of the distance between the cup and the plates was one of many factors which could affect flake size (as mentioned in EP 0 289 240), it was not appreciated that varying this distance could have a profound effect on the particle thickness size distribution and it is this particular characteristic of a product which is fundamental to the quality of the product. Indeed, it had been assumed that any significant increase of the cup-plate separation, beyond the median
15 at which an acceptable product is obtained, would lead to a deterioration of the product and in particular its flatness and any reduction simply reduced the nominal flake diameter. However, the surprising discovery is that the cup-plate separation can be substantially increased or decreased with a concomitant change in particle size distribution and without any other reduction in the quality of the product provided the
20 nominal thickness difference is compensated for by one of the other parameters. Furthermore, it is also an advantage that when increasing the cup-plate separation there is reduced wear on the plates which is caused by the interaction between the material being processed and the plate.

25 The cup-plate separation can be varied by up to 1500% from the minimum separation to obtain a suitable product. For instance, if the "normal" separation of the cup and the plates is 200 distance units then increasing the distance up to 500 units may obtain a wide particle size distribution or conversely reducing the distance to 100 units may give a much narrower particle size distribution.

Preferably the particle size distribution to be achieved by varying the distance between the cup and the plates is in the range from 10% to 95%, by which is meant that at 10%, then 95% of all particles are within a 10% size variation and at 95%, substantially all particles are within a 95% size variation.

5 It will be appreciated that, by adjusting the cup-plate separation, glass flake production can be carried out in such a way that the need to classify or grade and recycle glass flakes outside the desired particle size distribution can be substantially reduced or even eliminated.

10 The present invention also provides a process for forming flakes, as described above, which includes determining the separation between the cup and the plate at a distance such that the particle thickness size distribution is in the range 700 to 900 nanometres when set at approximately 100 units, and 700 to 1300 nanometres when set at 500 units thus allowing the apparatus to be operated in modes where the thickness particle size distribution can be varied to suit production/end use requirements.

15

Brief description of the drawings.

The accompanying drawings are as follows:

20 **Figure 1** shows graphically particle size distribution, obtained by varying cup-plate separations;

Figure 2 shows the different relationship between the edge of the spinning cup and plate entry; and

25 **Figures 3a and 3b** illustrate samples of particles produced as a result of different cup-plate separation.

Detailed description of the Invention

A process for producing glass flakes will now be described, by way of example, with reference to the accompanying drawings.

5 The process is essentially that described in EP 0 289 240 and makes use of apparatus also described and illustrated in this document. Figure 1 of the accompanying drawings shows how dramatically the particle size distribution can be changed by varying the separation between the cup 5 and the plates 9 (the item numbers are as used in EP 0 289 240). With the plates set at a distance from the cup which, having regard to all the other features and running conditions of the apparatus, is a minimum
10 in order to achieve a satisfactory product, the size distribution is that indicated by plot C. With such a size distribution, a considerable proportion of the glass flakes have a size more than 10% greater than the average or less than 10% lower than the average.

By decreasing the cup-plate separation from 500 units to 200 units, as illustrated in
15 plot B, substantially more of the particles are within the desired particle size distribution (10% from the average). Reducing the cup plate separation still further (to 100 units, as illustrated in plot A) reduces still further the proportion of particles outside the desired range (10% from the average).

Figure 2 shows, diagrammatically, the distances between the outer periphery of the
20 cup and the mouth of the plates, corresponding to plots A (100 units), B (200 units) and C (500 units) shown in Figure 1.

Figures 3a and 3b illustrate flakes obtained separations of 100 and 500 units respectively. It can be seen that the thickness of the flakes at 100 units separation is very uniform whereas there is considerable variation at 500 units separation.

25

A MEANS OF EFFECTING PARTICLE SIZE DISTRIBUTION IN GLASS FLAKE PRODUCTION

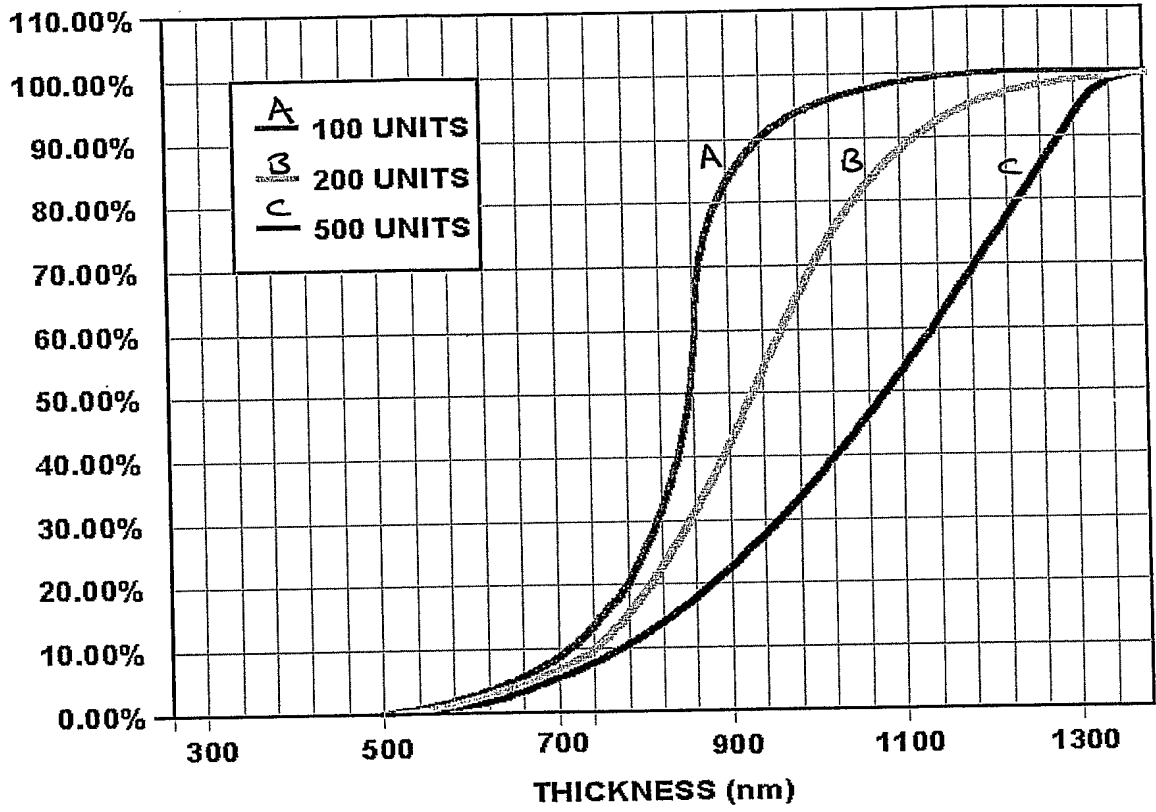


Fig. 1



Fig. 2

DIAGRAM SHOWING REPRESENTATION OF CUP TO ENTRY DISTANCE

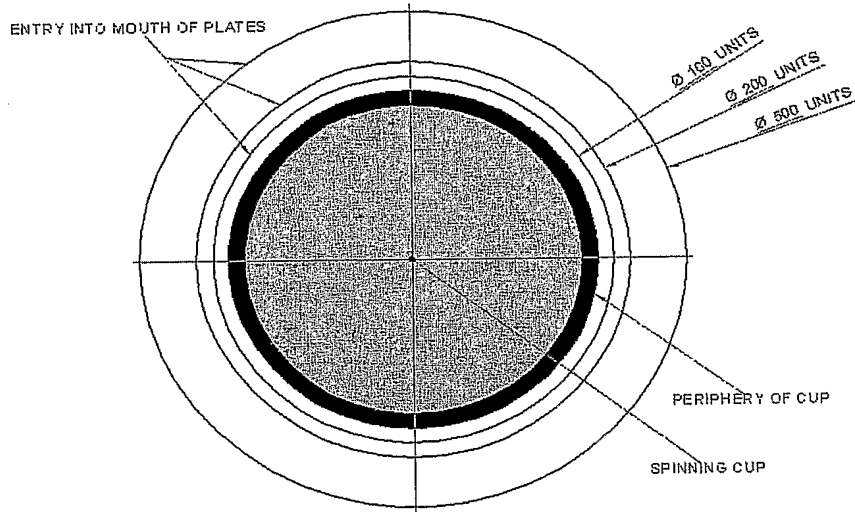
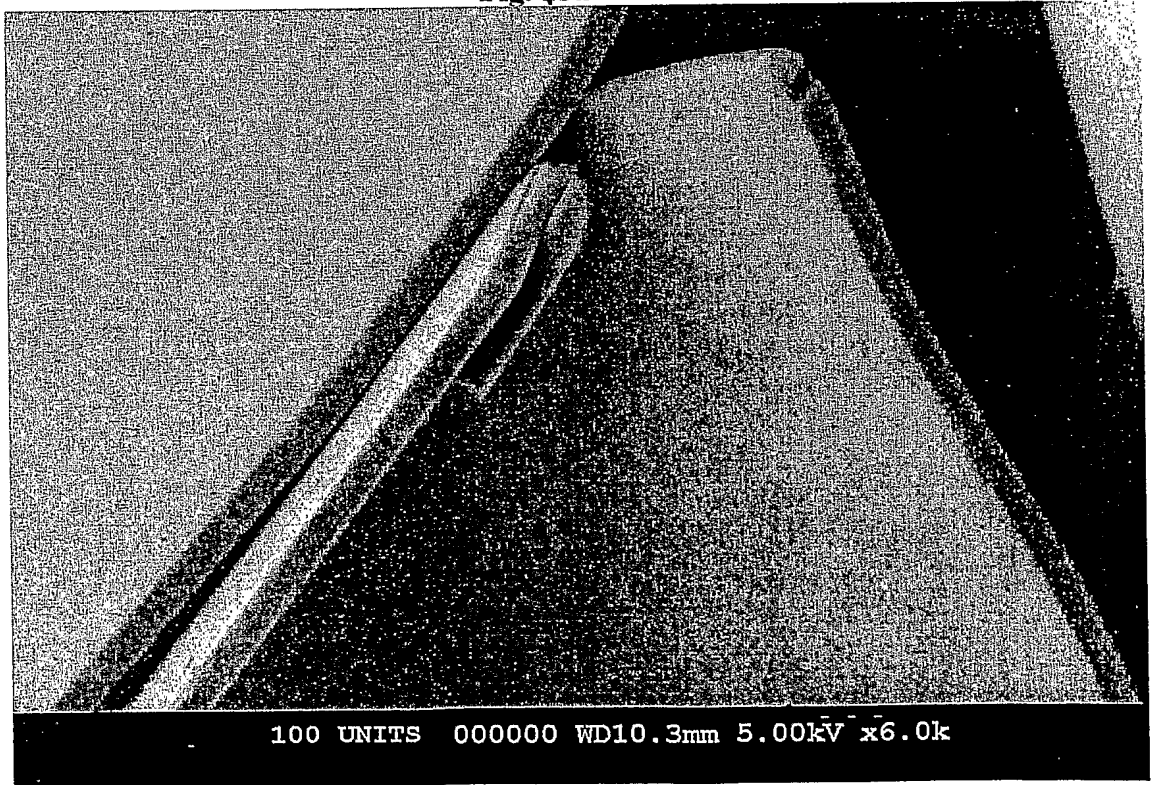


Fig. 43a





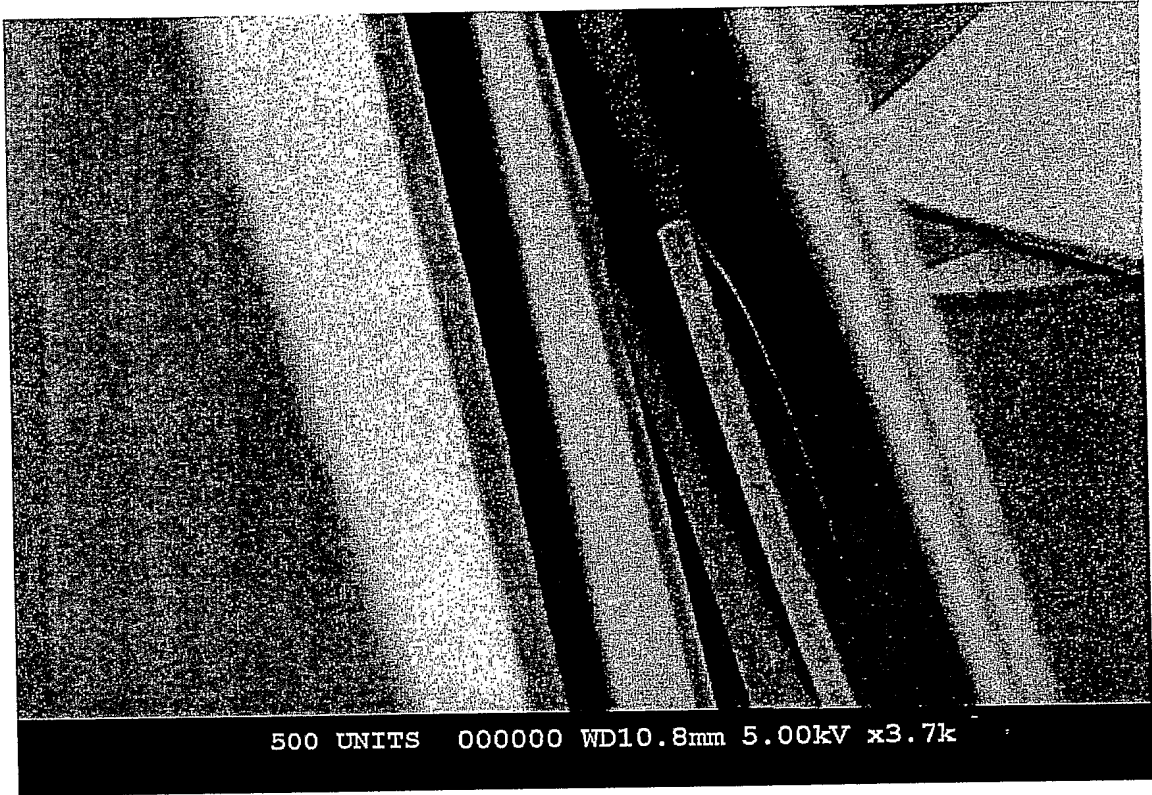


Fig. 3b

